Method for Separation of Coal Conversion Products from Sorbent/Oxygen Carriers Srivats Srinivasachar and Teagan Nelson **Envergex LLC**

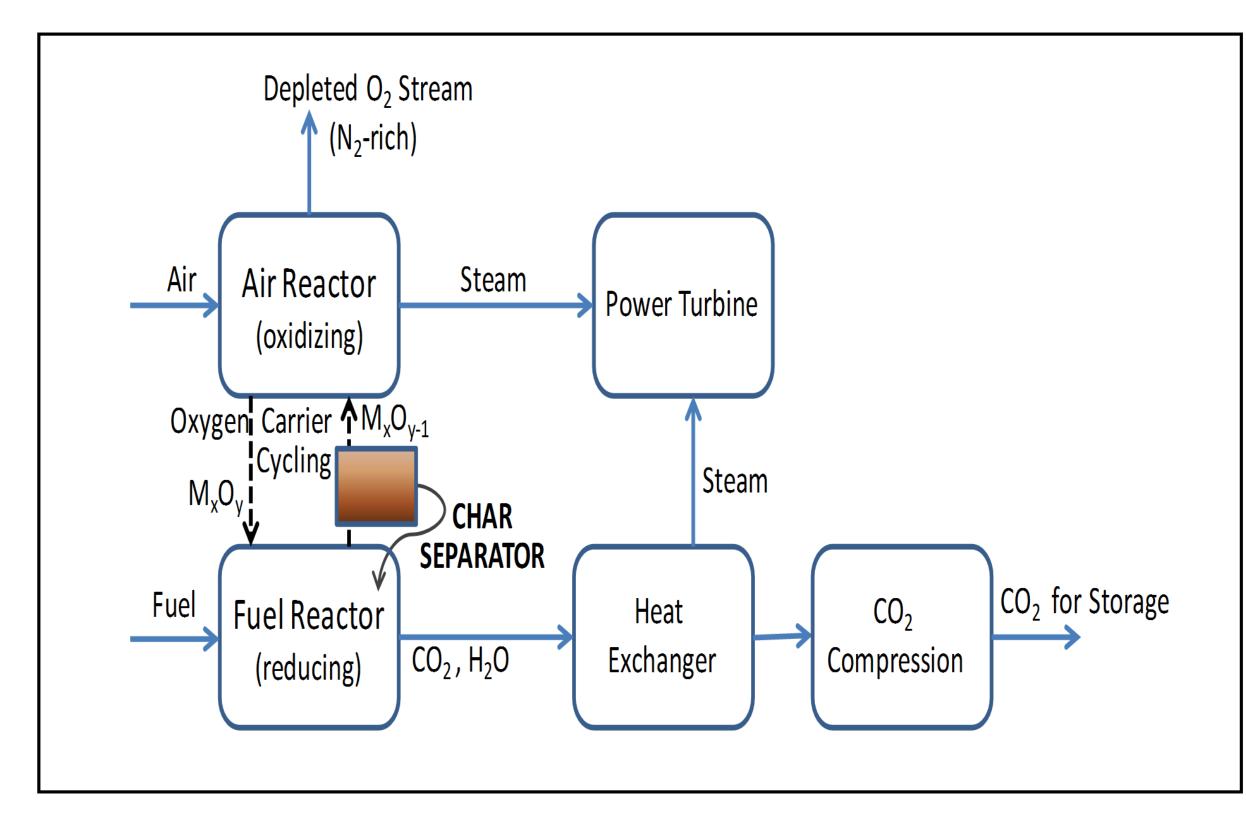


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Background - CO₂ Capture

Chemical-Looping-Combustion (CLC) is an innovative power generation technology that produces a near-pure CO₂ stream (carbon capture) at a lower cost and higher efficiency. Process consists of:

- Solid oxygen-carrier used to provide oxygen to fuel in fuel reactor
- Oxygen-depleted solids regenerated separately in air reactor
- Some of the challenges facing CLC development:
 - Unconverted char is entrained to air reactor and forms CO₂
 - This CO₂ is not captured Carbon Capture Rate (CCR) penalty.
 - Ash resulting from coal conversion can interact with and deactivate OC



Chemical Looping Combustion Process showing Char separator

Project Objectives and Methodology

> Objective: Develop a char separator to segregate fuel-based char and ash from solid oxygen-carrier before transport to air reactor

> Methodology

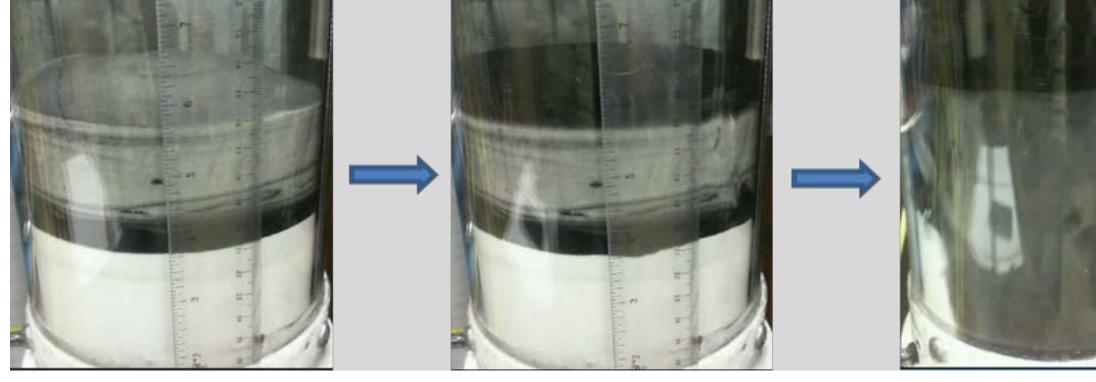
- Developed 2 separation technologies based on particle terminal velocity and density.
- Performed cold flow batch and continuous test to separate OC/char
- Developed a 100 lb/hr hot flow system to validate separation technologies.

Experimental Setup

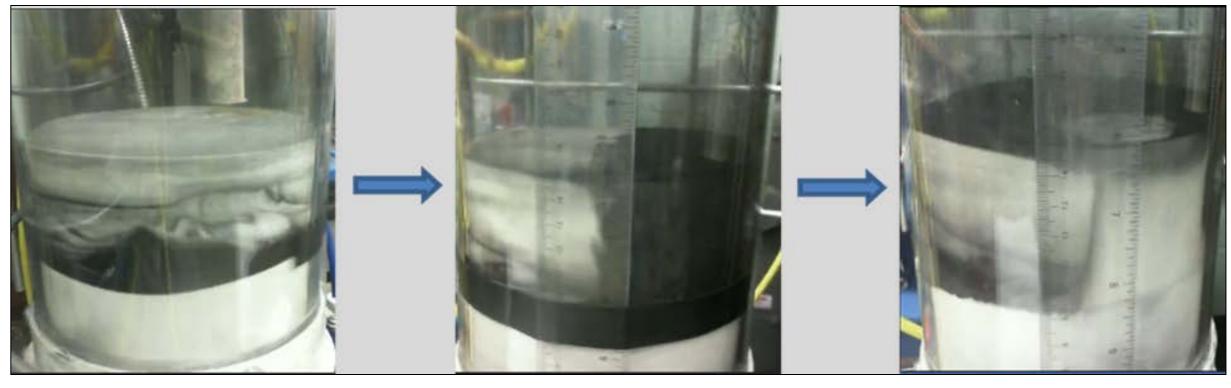
- Elutriation Beds (EB) based on terminal velocity separation
- Large char separator (LCS) used for density-based separation
- Constructed batch systems for proof-of-concept of technology; Used glass beads and carbon (activated carbon) as test medium. \succ Continuous flow (50 kg/hr) cold flow units constructed and
- tested; OC/char from a GE pilot unit and ilmenite/char used.

Results – Phase I

- For LCS performance, "control" was bubbling fluidized bed regime
- Significant back-mixing of the carbon observed during "control"
- > LCS showed good separation of carbon with no back-mixing



"Control" test showing carbon mixing behavior (left to right).



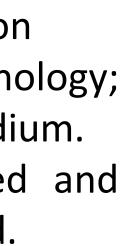
LCS test showing carbon segregating (left to right) with no mixing

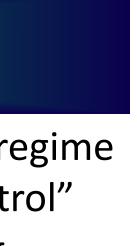
1 - Aller - La	Particle Size (µm)	Carbon Removed
	> 420	44%
SIN MARIA	1200 - 420	34%
x 1 and the	420 – 150	35%
	150 – 105	6.3%
	1< 105	12.9%
	> 100 Overall	35%
	Overall	25%

LCS test with GE OC/char mix. Char segregating to top (left); char removal performance for each size bin (right)

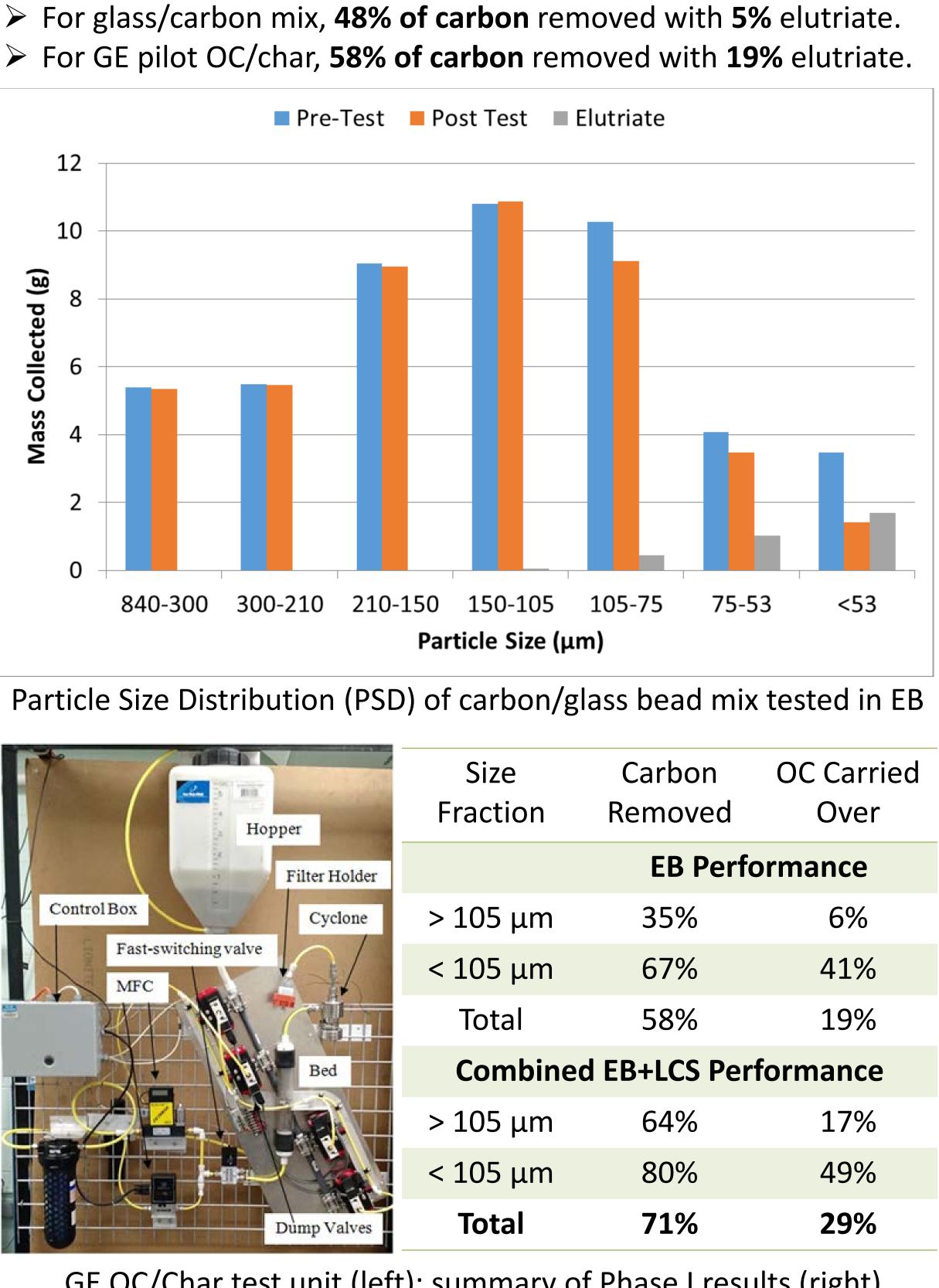


- > 30 cm/s EB bed velocity (minimize OC elutriation).







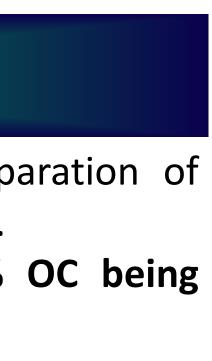


Hopper	Size Fraction	Carbon Removed	C
Control Box Cyclone		EB Perfe	orr
	> 105 µm	35%	
Fast-switching valve	< 105 µm	67%	
	Total	58%	
Bed	Combined EB+LCS Perfor		
	> 105 µm	64%	
	< 105 µm	80%	
Dump Valves	Total	71%	

GE OC/Char test unit (left); summary of Phase I results (right)

Phase I Discussion

- > Technology used for the LCS system facilitated separation of carbon from glass beads while minimizing back-mixing.
- > For EB, >45% carbon removal will result in >15% OC being segregated with carbon
- **EB** alone not suitable for segregating char from OC
- LCS upstream of EB will help reduce operating velocities in EB and minimize OC entrainment

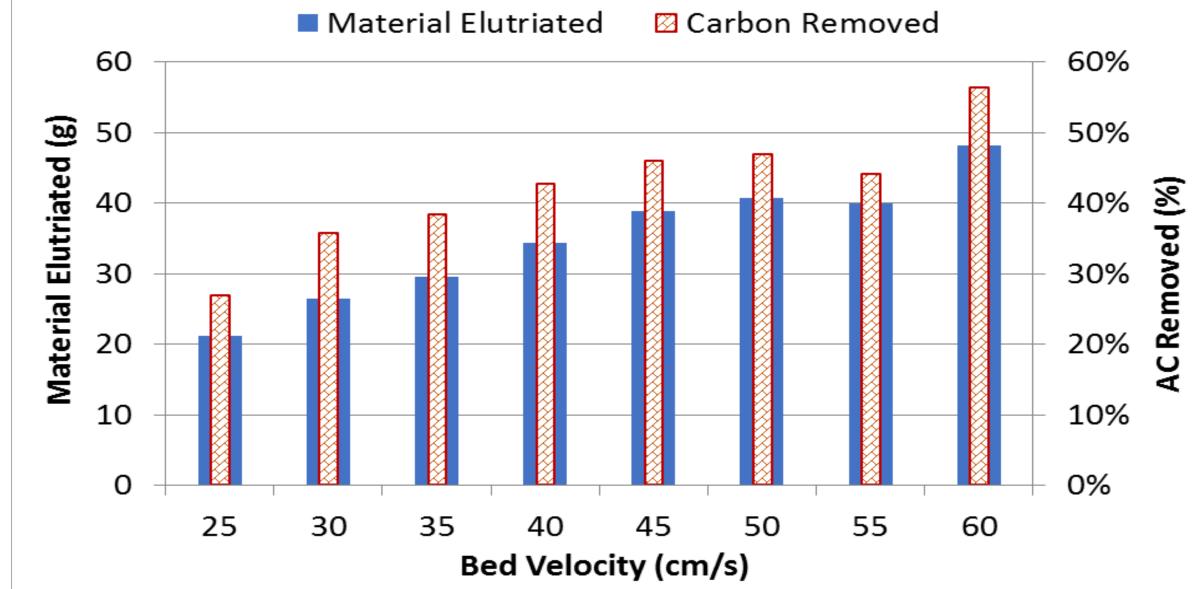


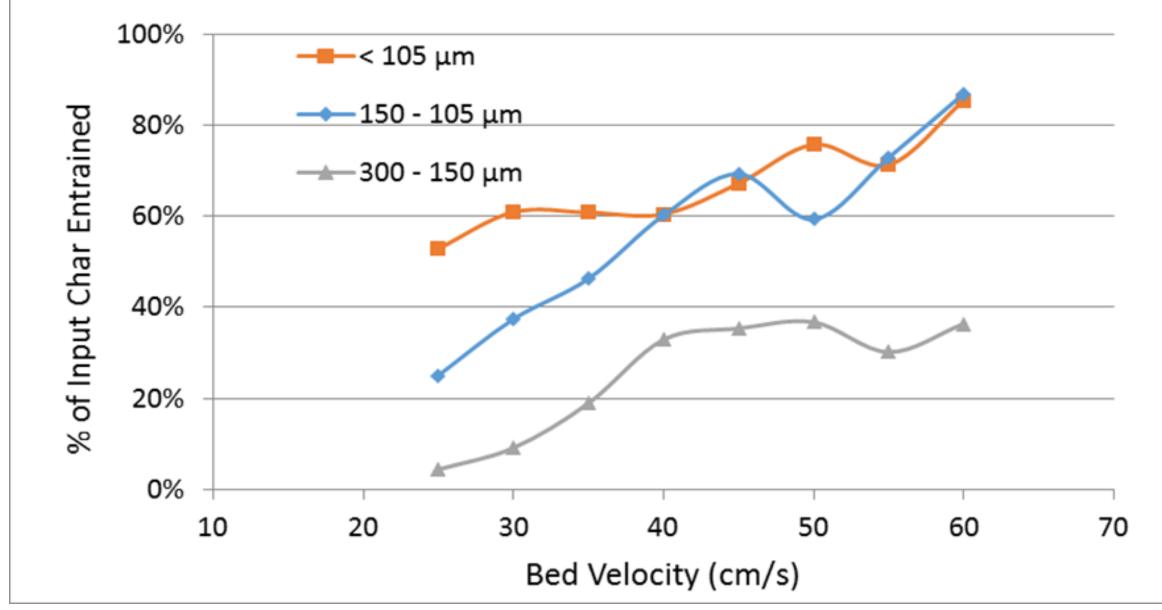
Results – Phase II

- For LCS system design changed to rectangular unit
- Char produced from a PRB coal using pyrolysis and gasification
- \succ Ilmenite/char PSD overlapped in the 150 to 350 μ m range
- Char segregated to top of bed and removed from top exit
- For EB, optimum bed velocity of 50-60 cm/s
- LCS-EB configuration identified as best order for char segregation





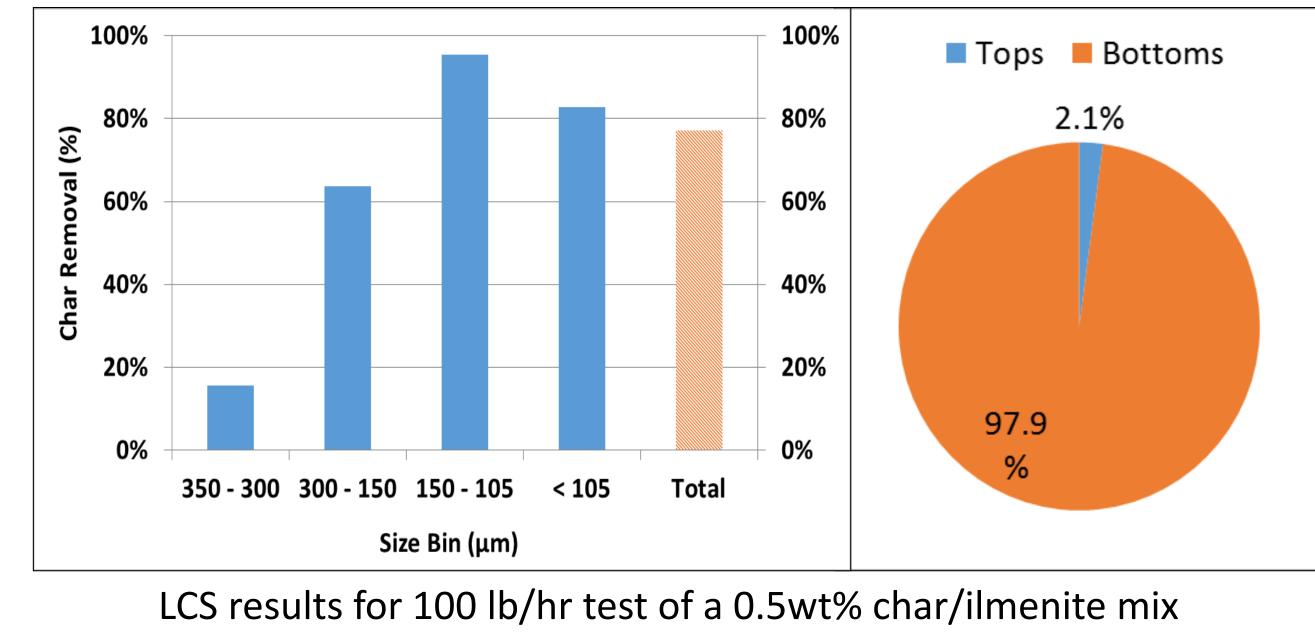


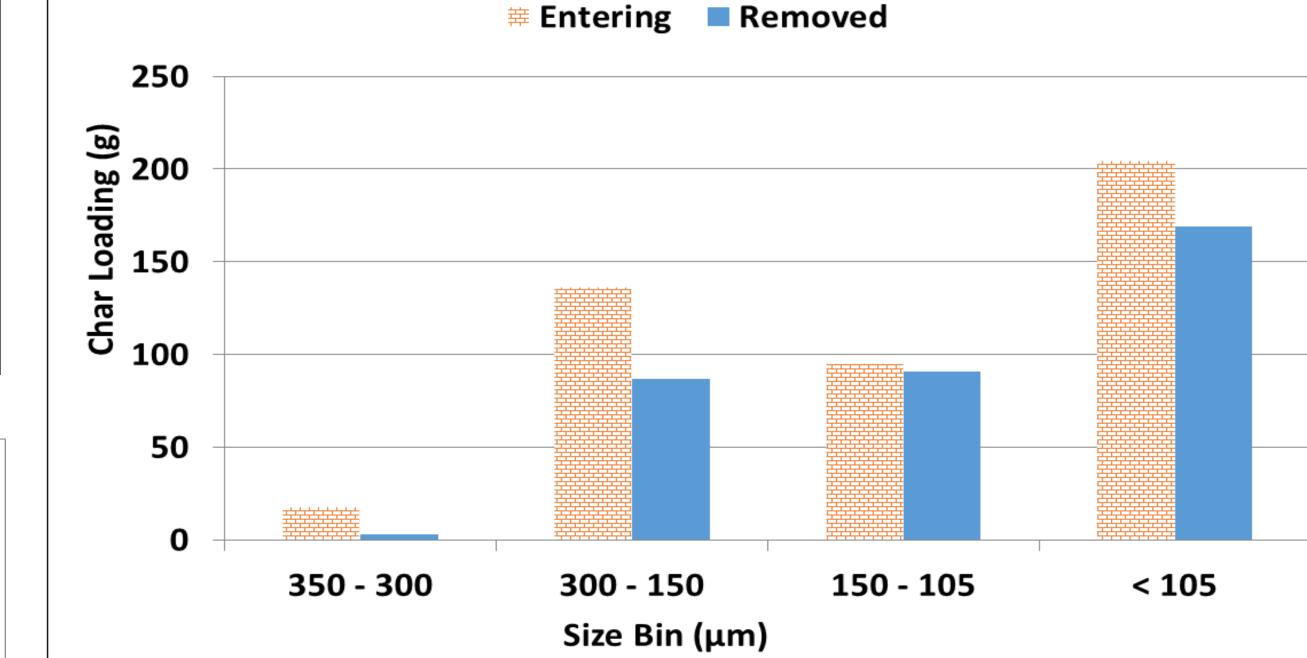


Elutriation vs Velocity for EB continuous unit (top); Char removal efficiency (bottom)

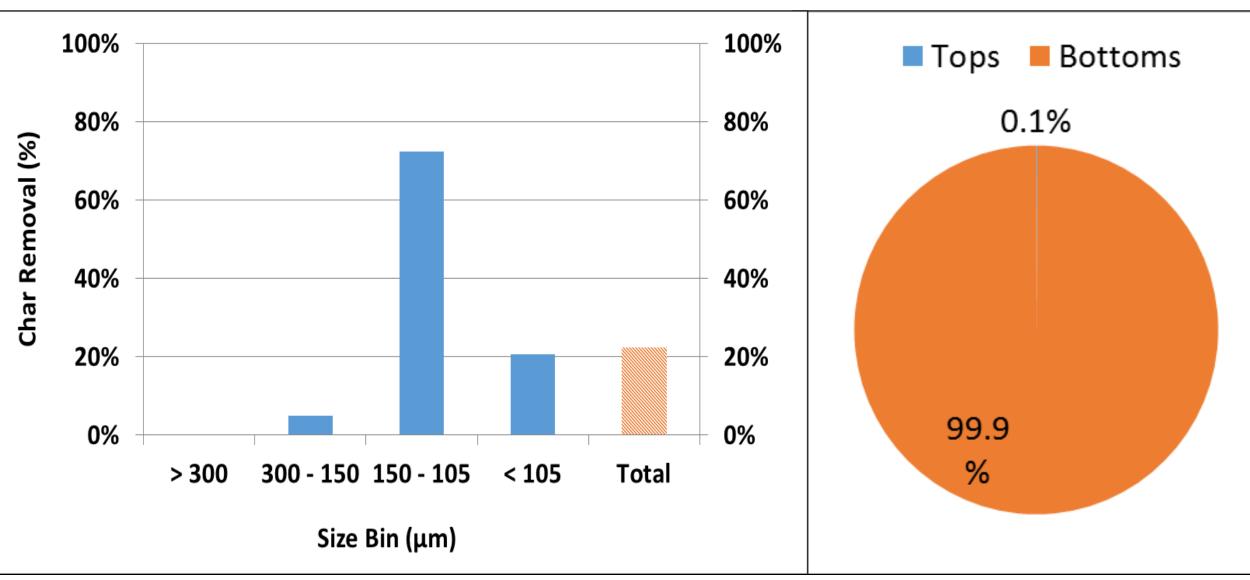
Future Work

- Construction of hot flow 100 lb/hr system (completed)
- \succ Hot flow testing of char/OC mix at CLC operating temperatures (800 900°C)
- Construction of cold-Flow 500 kg/hr system for future integration in an actual pilot CLC system





Distribution of Char Entering with and Removed from Ilmenite in LCS



EB results for 50 kg/hr test of a 0.5wt% char/ilmenite mix

Results – Continuous Test

Significant removal in LCS unit – 0.5% to 13% (26 X enrichment).

- Char removal by LCS of 77%
- Char removal by EB of 22%
- Combined removal for both LCs and EB of 82%

Acknowledgements

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Hot Flow Unit

Boiler

Separators

and some state of the

Completed Hot Flow Unit

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